Spermine Sepharose as a clustered-charge anion exchange adsorbent

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\textbf{A B S T R A C T}

We previously showed that the affinity and capacity of ion exchange adsorbents of a given total charge density are improved by immobilization of the charges in pre-ordered clusters, rather than individually in random locations. This previous work used pentalysaminamide and pentaargininamide as clustered ligands. This approach allows close control of cluster size, but is uneconomically expensive for some research and most practical applications. In this work, we demonstrate that the inexpensive synthetic analog of the natural polyamine spermine (H\textsubscript{2}N—CH\textsubscript{2}—CH\textsubscript{2}—NH—CH\textsubscript{2}—CH\textsubscript{2}—NH—CH\textsubscript{2}—CH\textsubscript{2}—CH\textsubscript{2}—NH\textsubscript{2}) also can serve as the basis of effective clustered adsorbents. The calcium-depleted form of the protein α-lactalbumin, and RNA from baker’s yeast, were adsorbed on a spermine Sepharose adsorbent. This adsorbent exhibited enhanced α-lactalbumin binding capacity (Q\textsubscript{max} > 1.6 and 1.3-fold higher than those for Qiagen DEAE and GE DEAE Sepharose adsorbents of much greater charge density) and higher initial binding affinity (Q\textsubscript{max}/K\textsubscript{D} 2.4 and 2.1-fold higher, respectively). The new spermine-based matrix exhibited a higher value of the Z parameter, suggesting an increased number of apparent interaction sites between the protein and the resin, and functioned well in column mode.

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1. Introduction

The steady increase in titers and sales of recombinant pharmaceutical proteins has increased interest in high-efficiency, high-capacity downstream processes for the recovery and purification of biological products [1–3], particularly since estimates of the fraction of bioprocess costs devoted to purification range as high as 80% [4–6]. The continuing need for selective, scalable and economical unit operations has driven the design of novel bioengineering strategies [7,8].

Chromatographic purification remains the most costly element of biopharmaceutical downstream processing [9,10], and development of optimal chromatographic processes is a central issue in bioprocess engineering. Because it offers strong and easily reversible protein adsorption, ion-exchange chromatography is widely used for the selective purification of biomolecules [11,12]. Traditional ion-exchange adsorbents present a random charge distribution over the particle surface that creates a heterogeneous field of adsorption sites [13]. In order to improve this random charge distribution for protein capture, adsorbents have been modified in the past to present improved characteristics by either increasing ligand density through the use of tentacular adsorbents [14,15] or by attaching polycations such as polyethyleneimine or polylysine in order to enhance product selectivity and recovery [16].

Many proteins present a characteristic high charge-density patch that can play a dominant role in the ion-exchange adsorption of these molecules [11,17–19]. We have found that an adsorbent displaying uniform clusters of positive charge shows a higher affinity and capacity for negatively charged biomolecules than an adsorbent with the same total charge density displayed as dispersed charges [11,20]. Clustered pentaargininamide adsorbents of relatively low ligand density show higher affinity for negatively charged proteins than conventional adsorbents of much higher ligand density [11]. The use of pentaargininamide as a ligand in research and for process scale purification, however, must contend with the cost and base-lability of the ligand, which hampers efficient resin cleaning. In this work we describe spermine as an inexpensive, stable ligand for clustered adsorbents. Spermine is a polycationic polycation involved in DNA packaging whose four amines (see Fig. 1) can form a cluster of four positive charges [21], and whose low cost and alkali stability make it potentially suitable as a ligand for clustered-charge anion exchange chromatography.
In the present work we demonstrate the superior affinity and capacity of a spermine Sepharose clustered-charge anion exchanger for the anionic protein α-lactalbumin, which presents a modifiable charge cluster. The clustered-charge adsorbent presents enhanced initial binding affinity \( (Q_{\text{max}}/K_0) \) and maximum binding capacity \( (Q_{\text{max}}) \) when compared to dispersed-charge commercial adsorbents, even when the latter have higher ligand density.

2. Materials and methods

2.1. Materials

Sephrose CL-6B, Q Sepharose Fast Flow and DEAE Sepharose were from GE Healthcare (Piscataway, NJ). DEAE Plasmid Plus resin was from Qiagen (Valencia, CA). All other reagents were from Sigma Aldrich (St. Louis, MO) including salmon sperm DNA (Cat. number: D1626), Baker’s yeast RNA (Cat. number: R6750) and Ca\(^{2+}\)-depleted α-lactalbumin from bovine milk (Cat. number: L6010). α-Lactalbumin was prepared from unpasteurized bovine milk and was purified by ion exchange chromatography on DEAE-agarose. Its purity is ≥85% as was determined by PAGE. The molar mass for the protein used was 14,100 g/mol and the extinction coefficient \( \varepsilon^{1%} = 20.1 \) \([22]\).

2.2. Adsorbent preparation

Aldehyde activation of Sepharose was based on the method of Miron and Wilchek \([23]\). For activation, DI water-washed Sepharose CL-6B (400 μl in 1.6 mL water) was treated with 0.2 M sodium periodate for 3 h at room temperature, then washed with DI water and resuspended in 50 mM borate buffer pH 9.5 ± 0.2. To 400 μl of activated Sepharose CL-6B settled resin, 1.6 mL of spermine tetrahydrochloride (45 mg/mL) solution in 50 mM borate buffer, pH 9.5 was added and incubated on a gyratory rotator at room temperature for 2 h and centrifuged 2 min at 16,000 × g. The gel with the bound spermine was treated for 3 h with 2 mL of 2 mM sodium borohydride in 50 mM borate buffer, pH 9.5 to reduce the initially formed Schiff base into a stable secondary amine linkage. Spermine modified Sepharose was washed with 20 mM phosphate buffer, pH 7.0 and stored at 4 °C.

2.3. Ligand density determination

The ligand density of spermine Sepharose was determined by titration with 5 mM NaOH in column mode using an ÄKTA purifier FPLC equipped with a post-column pH monitor. Spermine Sepharose was packed in a column (5 × 20 mm) and equilibrated with 5 column volumes of 0.1 M HCl, and then 5 mM NaOH was run through a bypass in order to equilibrate the extra-column volume. After the equilibration, 5 mM NaOH was passed through the column to determine the moles of base required to titrate the acidified adsorbent. The amount of 5 mM NaOH required for titration of unmodified Sepharose (typically about 1.2 mL) was subtracted from that required to titrate the spermine Sepharose (typically about 6.8 mL) to obtain the millimoles of NaOH used to titrate spermine.

2.4. Adsorption isotherm measurements

Aliquots (25 μl) of 60% (v/v) spermine Sepharose suspension in binding buffer (10 mM Tris, 10 mM NaCl, pH 8) were placed in 1.5 mL Eppendorf tubes. To these tubes different amounts of protein stock solution (10–180 μl of 5 mg/ml Ca\(^{2+}\)-depleted bovine α-lactalbumin (or RNA) in binding buffer) were added, followed by binding buffer up to 1 mL. Tubes were placed on a gyrotary rotator at room temperature for 1 h, then centrifuged for 10 min at 16,000 × g. Protein concentration in the supernatant was quantified by 280 nm absorbance using a Tecan Infinite M200 Pro microplate reader (Tecan, USA). The adsorbent pellets were washed with 1 mL of binding buffer followed by recentrifugation (the wash contained only a small fraction, 3.1% ± 1.7%, of the added protein). Bound protein was eluted with 1 mL of elution buffer (binding buffer + 1 M NaCl) and adsorbed protein content was determined. In order to determine the completeness of protein recovery, mass balances were performed by dividing the sum of the protein remaining in the supernatant after adsorption equilibration + protein recovered in the wash + protein in the elution fraction, by the original amount of protein added. Theionic strength of the 10 mM Tris buffer, 10 mM NaCl, pH 8 is estimated at 0.015 M.

2.5. Data analysis

The mass balance recoveries for all points in all experiments closed in the range 86–111%. Protein adsorption data were fit to the Langmuir (Eq. (1)), Langmuir–Freundlich (Eq. (2)) isotherms and the steric mass action (SMA) model of Cramer et al. (Eq. (3)) \([24]\).

\[
y = \frac{Q_{\text{max}}X}{K_0 + X} \tag{1}
\]

\[
y = \frac{Q_{\text{max}}X^{n_H}}{K^nH + X^nH} \tag{2}
\]

\[
y = \left( \frac{Q_r}{K} \right) \left( \frac{X}{A - (\nu + \sigma)Q_r} \right)^n \tag{3}
\]

In these equations, \( y \) is the bound protein concentration, \( X \) is the free protein concentration, \( Q_{\text{max}} \) is the maximum binding capacity (in μmol/ml of settled bed adsorbent), and \( K_0 \) is the dissociation constant. In Eq. (2), \( n_H \) is the Langmuir–Freundlich heterogeneity parameter. In Eq. (3), \( Q_r \) is the equilibrium adsorbent-bound protein concentration, \( K \) is the equilibrium constant, \( A \) is the total ionic capacity of the adsorbent in μmol/ml of settled bed adsorbent, \( \sigma \) is the dimensionless steric factor that reflects the number of sites on the surface that are shielded by the adsorbate and prevented from exchange with salt counter-ions in solution and \( \nu \) is the dimensionless characteristic charge that reflects the number of sites that the protein interacts with on the surface. Fitting used Igor Pro (WaveMetrics, Lake Oswego, OR; version 6.05) which uses the Levenberg–Marquardt algorithm to search for parameters which minimize the \( \chi^2 \) values, as described previously \([11,20]\). The initial guess vectors for the parameters were varied manually to ensure that a true global optimum was found.

Boardman and Partridge \([25]\) and Regnier \([26]\) have described the stoichiometric displacement model which emphasizes the importance of electrostatic interactions between proteins and adsorbents in terms of ionic equilibria. If an electrolyte such as NaCl is used, the equilibrium of Na\(^+\) ions and target proteins (a polygon represented by \( P^n^+ \)) between the mobile phase (\( m \)) and the adsorbent (\( ad \)) can be represented by: \( 2Na_{ad} + P_m \leftrightarrow P_{ad} + 2Na_m \). Beginning with this equilibrium an expression was derived which relates the binding affinity of the adsorbent to the mobility of the displacing salt in the mobile phase which was then linearized to the
form \[11,25,26]\: log \[K_i\] = Z log[NaCl] + log [I] where \(K_i\) is the initial binding affinity of the adsorbent, \(I\) is a constant and \(Z\) represents the number of counter ions displaced when a target protein is adsorbed on the resin surface. This also has been interpreted as the number of chemical interactions between the adsorbate and the adsorbent \[11,27\], though we have shown that \(Z\) can be fractional and can vary with temperature \[19\]. When the initial binding affinities of the proposed adsorbents at different NaCl concentrations are plotted, a \(Z\)-plot can be generated and the negative value of the slope of this graph gives the respective \(Z\) value. Finally, the \(Z\) values for adsorption of \(\alpha\)-lactalbumin on the proposed clustered adsorbent and a commercial non-clustered adsorbent (Qiagen DEAE) were calculated.

2.6. Column chromatography

Column chromatography experiments were performed using a glass column (21 mm H \(\times\) 5 mm ID) packed with the anion exchange adsorbent. The column was initially equilibrated with 5 column volumes (CV) of buffer A (10 mM Tris, 10 mM NaCl, pH 8.0). 1 ml of a protein mixture containing equal amounts of Ca\(^{2+}\) depleted \(\alpha\)-lactalbumin (0.2 mg) and bovine serum albumin (BSA; 0.2 mg) were loaded on the column. The column was washed with 5 CV of Buffer A (10 mM Tris, 10 mM NaCl, pH 8.0), then sample was eluted over 25 CV with a linear gradient from Buffer A to Buffer A + 250 mM NaCl. All experiments were carried out at 4 °C on an AKTA purifier 10 (GE Healthcare, Uppala, Sweden). The proteins were identified based on their retention times when run separately on the same column.

3. Results and discussion

3.1. Adsorbent preparation

The four \(pK_a\) values of spermine are 7.96, 8.85, 10.02, and 10.80, with the higher \(pK_a\) corresponding to the terminal amines \[21,28\]. We used SPARC to estimate that in the linkage created by conjugation of spermine to Sepharose by the periodate method \[OH–CH₂–CH₂–CH(OH)–O–CH₂–CH₂–H₂N–CH₂–…\] the \(pK_a\) of the coupled nitrogen is near 9.39; this implies that all four groups should be significantly protonated at the working pH of this investigation, pH 8.0. According to the Henderson–Hasselbalch equation, at pH 8.0, the spermine molecule conjugated to Sepharose has 3.3 charges/molecule.

In this initial work, we chose to prepare spermine Sepharose with a relatively low ligand density (typically 17 mM, 68 mM protonatable amines) in order to avoid a heterogeneous landscape of interacting adsorption sites as found in traditional ion exchange adsorbents. As mentioned above \[11\], clustered-charge adsorbents such as the spermine Sepharose used in this work, differ from the tentacular ion exchange adsorbent matrix \[11,14\]. In a tentacular ion exchange adsorbent, accessibility of the ligand is improved by using long linear polymer chains, which carry the functional ligands. In the case of clustered-charge adsorbents like spermine Sepharose, the ligand itself is a small charged polymer which forms a cluster of positive charges.

Sepharose CL-6B was chosen as a base matrix since it offers a hydrophilic surface and can be easily activated with sodium periodate to a controlled degree, as reported elsewhere \[23\]. The terminal amines of spermine have \(pK_a\)s of 10.02 and 10.8, and the internal amines have \(pK_a\)s 7.96 and 8.85 \[28\]. In order to achieve low ligand density by rendering some potentially reactive amines charged and unreactive, spermine was coupled at pH 9.5 ± 0.2.

3.2. Adsorption isotherm measurements

\(\alpha\)-Lactalbumin is a popular model system for study of protein adsorption and chromatography \[29–31\]. Like at least 30% of eukaryotic proteins \[32\], it is a molten globule under physiological conditions, but it is compact and not hydrophobic \[33–36\]. \(\alpha\)-Lactalbumin has a conserved Ca\(^{2+}\) binding domain (dissociation constant of 10\(^{-7}\) M) \[37\], rich in aspartate residues located at the interface between the two subdomains of the protein \[38\]. In the Ca\(^{2+}\)-depleted form of \(\alpha\)-lactalbumin, repulsion among these residues increases the solvent accessibility of this anionic charge patch.

The maximum binding capacity (\(Q_{\text{max}}\)) and initial binding affinity (\(Q_{\text{max}}/K_D\)) were compared for the spermine Sepharose adsorbent and for conventional commercial adsorbents. As shown in Fig. 2 and Table 1, the lower-ligand-density (17 mM ligand) charge-clustered spermine Sepharose adsorbent gave a higher protein binding capacity (\(Q_{\text{max}} = 0.8 ± 0.1\) mM) and initial binding affinity (\(Q_{\text{max}}/K_D = 0.17\)) than DEAE Sepharose adsorbent (with 125 mM charge density \[20\]; \(Q_{\text{max}} = 0.5 ± 0.04\) mM; \(Q_{\text{max}}/K_D = 0.07\)) and the GE DEAE Sepharose (with 135 mM charge density; \(Q_{\text{max}} = 0.6 ± 0.08\) mM; \(Q_{\text{max}}/K_D = 0.08\)).

The much lower ligand and charge density of the spermine adsorbent should be emphasized in these comparisons, as it strongly affects protein adsorption \[39\]. Wu and Walters \[40\] established that increased ligand density increased lysozyme adsorption in carboxylate-based cation-exchange supports. This behavior has also been discussed for large molecular weight molecules such as monoclonal antibodies \[41\]. For the GE DEAE Sepharose adsorbent tested, the average through-space distance (which probably slightly over-estimates the actual distance because ligands often are somewhat confined to a specific surface area) between ligands is 23 Å vs. 46 Å for the spermine Sepharose adsorbent. The equivalent spherical diameter for \(\alpha\)-lactalbumin is 32 Å \[42\], which could imply that the commercial adsorbent forms an increased number of interactions with the target molecule as compared to spermine Sepharose. Nevertheless, the more widely separated ligands of the spermine Sepharose resin show higher affinity and binding capacity than the GE DEAE resin, supporting the idea that the clustered-charge approach provides enhanced protein adsorption. It is worthy of note that if the ligand density of the clustered spermine adsorbent were increased to densities typical of commercial adsorbents, interactions between ligands would create a more complicated landscape of adsorption sites. Every charge, however,
would be located in a cluster energetically competent to serve as a functional adsorption site.

The low ligand density used raises the possibility that the ligands may be localized to the outer layers of the agarose particles. We do not, however, expect the formation of ligand clusters which significantly modify adsorption behavior, based on the following calculation: Assuming that the spermine ligand is only localized in the outer 3% of the radius of the beads (mean bead diameter is 90 μm) the average inter-ligand distance would be 20.4 Å, whereas assuming uniform ligand distribution the average inter-ligand distance would be 46.1 Å. Given that the equivalent spherical diameter of α-lactalbumin protein is 32 Å [42], in either case at a given spot there would be no more than two ligands that could interact with the protein, except at rare statistical clusters which would not support the observed protein capacity.

We also analyzed the adsorption data by the steric mass action (SMA) model of Cramer et al. [24] which is based on the stoichiometric displacement model of Regnier et al. [43] (Table 2). Fitting of the 4-parameter SMA model to the data set gave consistent convergence. To resolve this issue, we set as initial guesses in the SMA fitting, the Langmuir Qmax and K0 parameters as SMA Q0 and K, respectively and estimated values of v and σ values. The SMA steric factor (σ), which reflects the number of sites on the surface shielded by an adsorbed protein, is 10-fold lower for spermine Sepharose than for the GE and Qiagen DEAE adsorbents, which have 7.9 and 7.4-fold higher ligand densities, respectively. We ascribe most of this difference to the difference in ligand density, any effect of clustering would best be determined using a spermine adsorbent of much higher ligand density, at which inter-ligand interactions might, however, become important.

Salt effects upon protein binding also were studied. Fig. 3a and b present α-lactalbumin adsorption isotherms at four different NaCl concentrations (10–60 mM). At the lower salt concentrations tested (10 and 26 mM NaCl), both the initial binding affinity (Qmax/K0) and maximum binding capacity (Qmax) were higher for the spermine adsorbent when compared to the Qiagen DEAE: 2.4 and 1.3 fold higher in Qmax/K0 at 10 and 26 mM and 1.6 and 1.2 fold higher in the maximum binding capacity. For the 40 and 60 mM NaCl concentrations, the initial binding affinity was higher for the DEAE adsorbent; clustered spermine adsorbent exhibits an increased sensitivity to salt concentration. This characteristic is important in elution-based chromatography since a stronger dependence of adsorption affinity on salt concentration may imply higher resolution capabilities in column mode chromatographic operations.

Salt concentration effects can also be described by the Z plot derived from the stoichiometric displacement model [40,44], as presented in Fig. 4. This graphical representation often exhibits a linear relationship between the logarithm of the initial binding affinity (Qmax/K0) of an adsorbent and the logarithm of the salt concentration employed. The slope for this plot gives the apparent numbers of interaction sites, Z, of the protein surface with the stationary phase. In our original investigation of clustered adsorbents, the α-lactalbumin Z value for pentalysinamide was 1.4 ± 0.2 (vs. 1.2 ± 0.2 for the unclustered monolysinamide adsorbent of the same total charge) and that for pentaargininamide was 1.0 ± 0.1 (vs. 0.3 ± 0.1 for the non-clustered monoargininamide of the same total charge).

**Table 1**
Values of Langmuir isotherm parameters Qmax and K0 and Langmuir–Freundlich Qmax and K0 parameters and heterogeneity parameter nH, for adsorption of α-lactalbumin (Ca2+ depleted) on spermine-Sepharose, DEAE Qiagen and GE DEAE Sepharose adsorbents.

<table>
<thead>
<tr>
<th>Resin</th>
<th>Langmuir isotherm parameters</th>
<th>Langmuir Freundlich parameters</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Qmax (mM)</td>
<td>K0 (μM)</td>
</tr>
<tr>
<td>Spermine Sepharose</td>
<td>10 mM NaCl</td>
<td>0.8 ± 0.1</td>
</tr>
<tr>
<td></td>
<td>26 mM NaCl</td>
<td>0.6 ± 0.1</td>
</tr>
<tr>
<td></td>
<td>40 mM NaCl</td>
<td>0.9 ± 0.4</td>
</tr>
<tr>
<td></td>
<td>60 mM NaCl</td>
<td>0.5 ± 0.2</td>
</tr>
<tr>
<td>DEAE Qiagen</td>
<td>10 mM NaCl</td>
<td>0.5 ± 0.1</td>
</tr>
<tr>
<td></td>
<td>26 mM NaCl</td>
<td>0.5 ± 0.04</td>
</tr>
<tr>
<td></td>
<td>40 mM NaCl</td>
<td>0.4 ± 0.03</td>
</tr>
<tr>
<td></td>
<td>60 mM NaCl</td>
<td>0.3 ± 0.01</td>
</tr>
<tr>
<td>DEAE GE Healthcare</td>
<td>10 mM NaCl</td>
<td>0.6 ± 0.1</td>
</tr>
</tbody>
</table>

Fig. 3. Adsorption isotherms of α-lactalbumin (Ca2+ depleted) on (a) DEAE Qiagen resin and (b) spermine Sepharose at 25 °C in 10 mM Tris, pH 8 at 10 mM NaCl (●), 26 mM NaCl (▲), 40 mM NaCl (□) and 60 mM NaCl (●). Error bars reported refer to the mean ± 1 SD.
Steric mass action model parameters $Q_\text{s}$, $K$, $L$, $\sigma$ (steric factor) and $\nu$ for adsorption of $\alpha$-lactalbumin (Ca$^{2+}$ depleted) on spermine Sepharose, DEAE Qiagen and GE DEAE Sepharose adsorbents.

<table>
<thead>
<tr>
<th>Resin</th>
<th>$Q_\text{s}$ (mM)</th>
<th>$K$ (mM)</th>
<th>$L$ (mM)</th>
<th>$\sigma$</th>
<th>$\nu$</th>
</tr>
</thead>
<tbody>
<tr>
<td>Spermine Sepharose</td>
<td>0.8 ± 0.1</td>
<td>4.7 ± 2.0</td>
<td>17 ± 0.4</td>
<td>21 ± 0.1</td>
<td>0.4 ± 0.6</td>
</tr>
<tr>
<td>10 mM NaCl</td>
<td>0.6 ± 0.1</td>
<td>13.3 ± 2.7</td>
<td>17 ± 0.4</td>
<td>28 ± 0.1</td>
<td>0.5 ± 0.1</td>
</tr>
<tr>
<td>26 mM NaCl</td>
<td>0.9 ± 0.4</td>
<td>73.4 ± 40.1</td>
<td>17 ± 0.4</td>
<td>17 ± 0.8</td>
<td>0.7 ± 0.1</td>
</tr>
<tr>
<td>40 mM NaCl</td>
<td>0.5 ± 0.2</td>
<td>71.2 ± 46.9</td>
<td>17 ± 0.4</td>
<td>31 ± 0.5</td>
<td>0.7 ± 0.1</td>
</tr>
<tr>
<td>DEAE Qiagen</td>
<td>0.5 ± 0.1</td>
<td>7.4 ± 1.7</td>
<td>125 ± 5</td>
<td>239 ± 0.6</td>
<td>0.4 ± 0.1</td>
</tr>
<tr>
<td>10 mM NaCl</td>
<td>0.5 ± 0.04</td>
<td>14 ± 2.7</td>
<td>125 ± 5</td>
<td>261 ± 0.3</td>
<td>0.5 ± 0.1</td>
</tr>
<tr>
<td>26 mM NaCl</td>
<td>0.4 ± 0.03</td>
<td>12.9 ± 2.4</td>
<td>125 ± 5</td>
<td>338 ± 0.6</td>
<td>0.5 ± 0.1</td>
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<tr>
<td>40 mM NaCl</td>
<td>0.3 ± 0.01</td>
<td>9.6 ± 1</td>
<td>125 ± 5</td>
<td>430 ± 0.2</td>
<td>0.4 ± 0.1</td>
</tr>
<tr>
<td>60 mM NaCl</td>
<td>0.6 ± 0.1</td>
<td>7.5 ± 2.6</td>
<td>135 ± 25</td>
<td>211 ± 0.7</td>
<td>0.5 ± 0.1</td>
</tr>
<tr>
<td>DEAE GE Healthcare</td>
<td>0.6 ± 0.1</td>
<td>7.5 ± 2.6</td>
<td>135 ± 25</td>
<td>211 ± 0.7</td>
<td>0.5 ± 0.1</td>
</tr>
</tbody>
</table>

We confirmed the high pseudospecific affinity of spermine agarose for (salmon sperm) DNA (results not shown), and also measured the adsorption of (total baker’s yeast) RNA on spermine adsorbents, where ion-exchange interactions would be expected to dominate. As shown in Fig. 5 and Table 3, spermine Sepharose showed a higher RNA binding capacity ($Q_{\text{max}} = 9.2 ± 0.9$ mg/mL adsorbent) and a higher binding affinity ($Q_{\text{max}}/K_D = 642$ mL/mg adsorbent) than a 1.2 mM pentaargininamide adsorbent previously developed ($Q_{\text{max}} = 2.1 ± 0.1$ mg/mL adsorbent; $Q_{\text{max}}/K_D = 395$ mL/mg adsorbent) [20]. Finally, in terms of economic comparison, spermine represents a much more economical approach to synthesis of clustered-charge adsorbents than pentaargininamide.

3.3. Column chromatography

To show the applicability of spermine Sepharose in column mode we demonstrated the separation of two anionic proteins using spermine Sepharose (ligand density 13.2 ± 0.4 mM or charge density 52.8 mM) and compared its separation efficiency with GE DEAE (ligand density 135 ± 25 mM) (Fig. 6). 1 ml of a mixture of $\alpha$-lactalbumin (0.2 mg; pl: 4.5, with a surface charge cluster) and BSA (0.2 mg; pl 4.7) was loaded on the column and eluted with a salt gradient. On the spermine Sepharose column, $\alpha$-lactalbumin elutes at 127 mM NaCl and BSA elutes at 184 mM NaCl whereas on GE DEAE $\alpha$-lactalbumin elutes at 125 mM NaCl and BSA elutes at 175 mM NaCl. This confirms that spermine Sepharose performs well in column chromatography, even at low ligand densities.

![Fig. 4](image1.png)  
**Fig. 4.** Z plots for determining the value of the stoichiometric displacement parameter $Z$ for adsorption of $\alpha$-lactalbumin (Ca$^{2+}$ depleted) on spermine Sepharose (●) and DEAE Qiagen (▲) in 10 mM Tris, pH 8 at 10, 26, 40 and 60 mM NaCl. $Z_{\text{spermine}}$: 2.2 ± 0.3 and $Z_{\text{DEAE}}$: 0.3 ± 0.02.

![Fig. 5](image2.png)  
**Fig. 5.** Adsorption isotherms of Baker’s yeast RNA. Langmuir fits for S Sepharose resin (O), Spermine Sepharose (●), Pentaargininamide adsorbent (▲), GE DEAE (●), and Qiagen DEAE resin (●) at 25 °C in 10 mM Tris, 10 mM NaCl at pH 8.0. (Results other than spermine Sepharose from Reference [20]).
Table 3
Values of Langmuir isotherm parameters \( Q_{\text{max}} \) and \( K_0 \) for adsorption of Baker's yeast RNA on QiaGen DEAE resin, GE DEAE Sepharose, pentaarginimide adsorbents (Arg5; 1.2 mM ligand density), spermine Sepharose and Q Sepharose at 25 °C in 10 mM Tris, 10 mM NaCl at pH 8.0. (Results other than spermine Sepharose from Reference [20]).

<table>
<thead>
<tr>
<th>Adsorbent</th>
<th>( Q_{\text{max}} ) (mg/mL adsorbent)</th>
<th>( K_0 ) (( \mu )g/mL)</th>
</tr>
</thead>
<tbody>
<tr>
<td>QiaGen DEAE (125 ± 5 mM)</td>
<td>1.6 ± 0.2</td>
<td>109 ± 27</td>
</tr>
<tr>
<td>GE DEAE Sepharose (135 ± 25 mM)</td>
<td>2.7 ± 0.8</td>
<td>192 ± 92</td>
</tr>
<tr>
<td>Pentaarginimide adsorbent (1.2 mM, 6 mM charge)</td>
<td>2.1 ± 0.1</td>
<td>5.3 ± 0.1</td>
</tr>
<tr>
<td>Spermine Sepharose (4.5 ± 0.4 mM, 18 mM charge)</td>
<td>9.2 ± 0.9</td>
<td>14.3 ± 3.2</td>
</tr>
</tbody>
</table>

Fig. 6. Linear gradient elution chromatography on spermine Sepharose (13.2 ± 0.4 mM ligand or 52.8 mM charge) and GE DEAE (135 ± 25 mM) of Ca\(^{2+}\) depleted α-lactalbumin and BSA. 0.4 mg (1 ml) of protein containing equal amounts of Ca\(^{2+}\) depleted α-lactalbumin and BSA were loaded onto a 21 mm H × 5 mm ID column on an AKTA purifier 10 (GE Healthcare, Uppsala, Sweden). The columns were washed with 5 CV of Buffer A (10 mM Tris, 10 mM NaCl pH 8.0), then eluted over 25 CV with a linear gradient from Buffer A to Buffer A + 250 mM NaCl. On spermine Sepharose α-lactalbumin elutes at 127 mM NaCl whereas BSA elutes at 184 mM NaCl. The proteins were identified based on their retention times when run separately on the same column; absorbance during regeneration with 1 M NaCl was negligible.

4. Conclusions

A clustered-charge spermine Sepharose adsorbent shows high affinity and capacity of protein adsorption even at low ligand densities, and performs well in a column chromatographic separation. The spermine Sepharose adsorbent exhibits higher salt dependency for protein adsorption than conventional DEAE QiaGen adsorbents, raising the possibility of improved resolution of closely related proteins employed in a column mode. Spermine also is more attractive than previous clustered adsorbents in terms of alkali stability and ligand cost. Finally, the high affinity and selectivity of spermine Sepharose support the idea that charge clusters play an important role in ion-exchange adsorption, even on conventional adsorbents.

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